

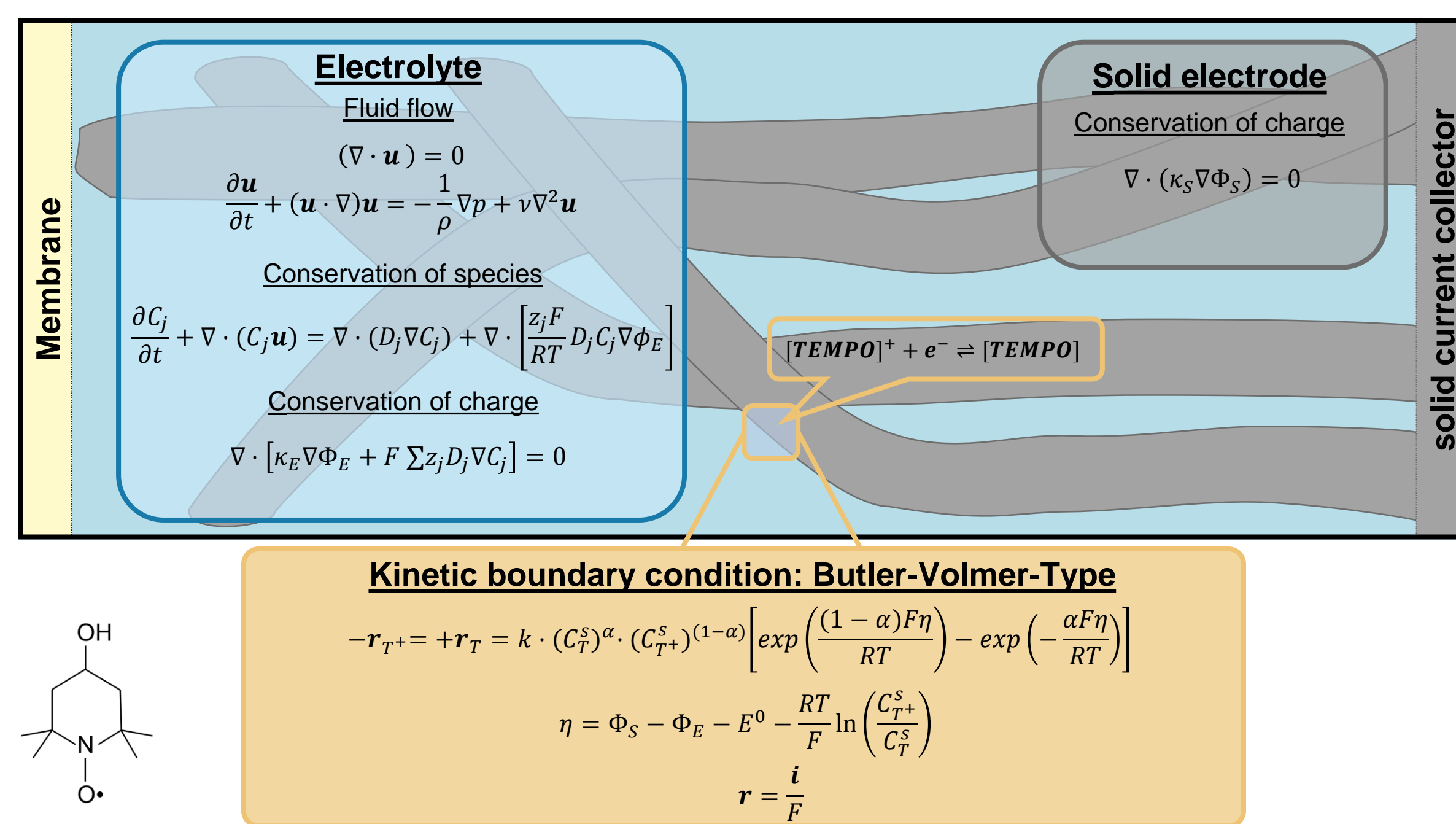
# A Multi-scale Flow Battery Modeling Approach Using Mass Transfer Coefficients<sup>[1]</sup>

Amadeus Wolf<sup>1</sup>, Emmanuel Baudrin<sup>2</sup>, Hermann Nirschl<sup>1</sup>

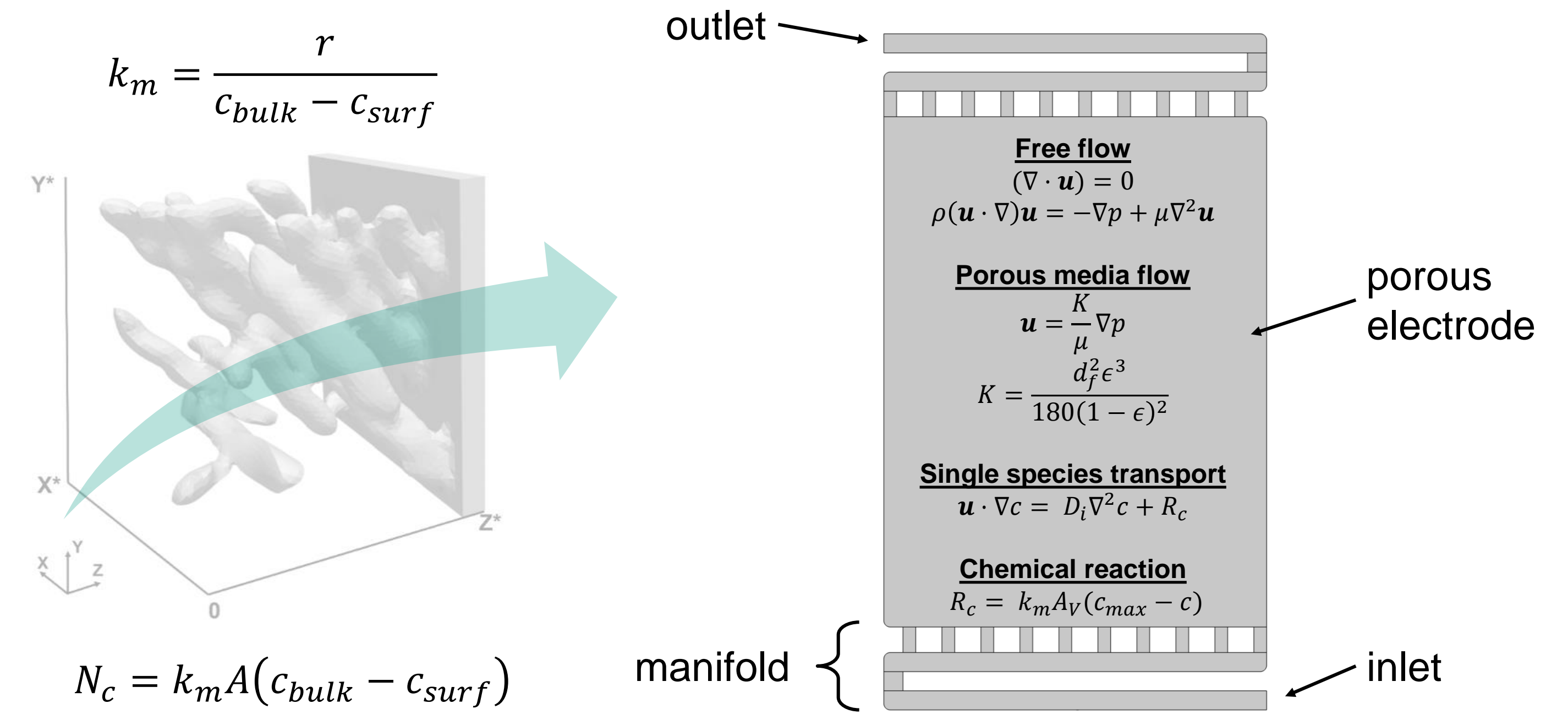
<sup>1</sup> Institute of Mechanical Process Engineering and Mechanics, Karlsruhe Institute of Technology, Germany

<sup>2</sup> Laboratoire de Réactivité et Chimie des Solides, Université de Picardie Jules Verne, Amiens, France

## 3D Resolved Micro-scale Model <sup>[2]</sup> (MSM)



## 2D Homogenized Cell Scale Model (HCSM)



### Motivation

Vague description of the mass transfer coefficient  $k_m$  in homogenized cell scale models. Mostly as empirical relation to velocity.

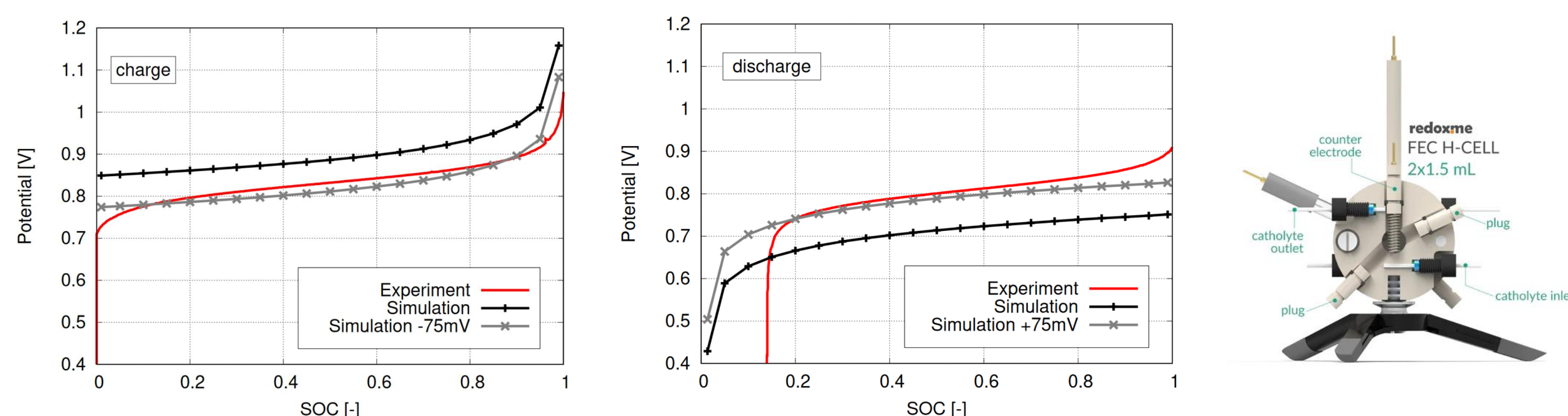
### Research Objective

Development of a method to extract  $k_m$  from MSM and subsequent usage in the HCSM. Comparison to empirical relations from literature.

### Approach

Obtainment by using reaction rate at distinct concentration level and discharge rate of the MSM, as well as resolved of bulk and surface concentration. Implementation of  $k_m$  in the HCSM as function of SOC and velocity.

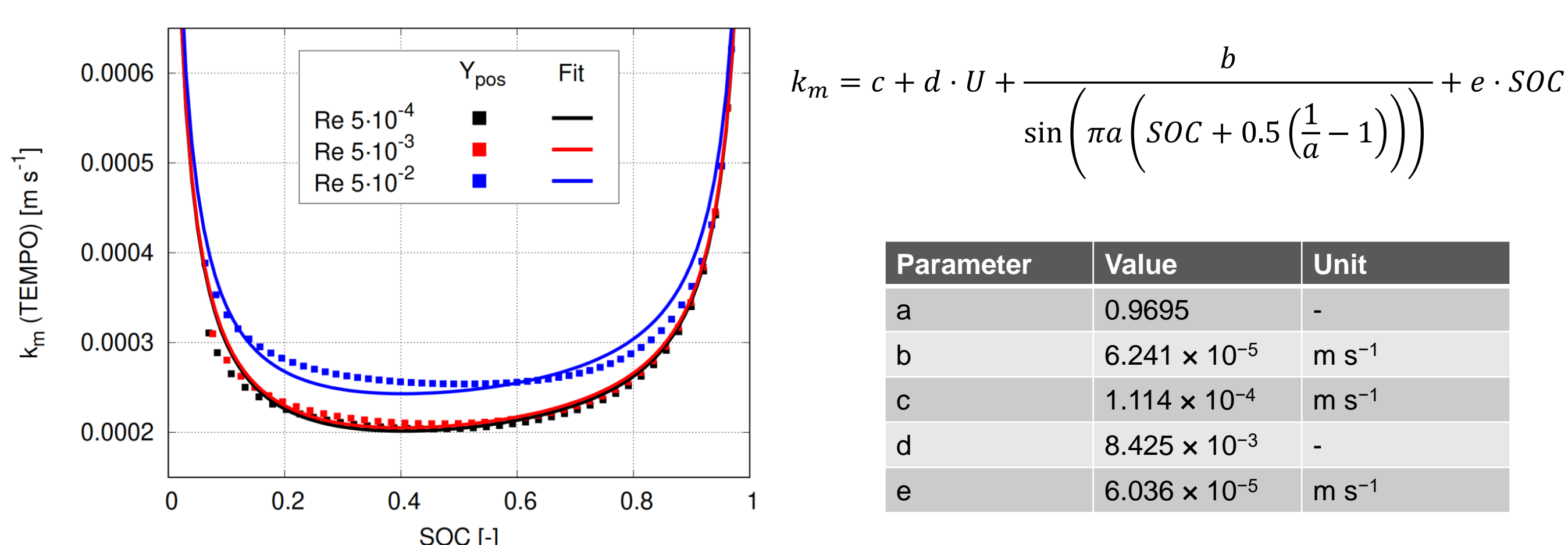
## Experimental Validation of the MSM



Potential vs SOC for the first charge (left) and first discharge (right) cycle of the redoxme FEC H-Cell. Independent measurements of half-cell potentials. The current density is  $2.83 \text{ mA cm}^{-2}$ , the concentration is  $0.011 \text{ M TEMPO}$  in  $1 \text{ M NaCl}$  and the flow rate is  $30 \text{ mL min}^{-1}$  ( $0.0177 \text{ m s}^{-1}$ ).

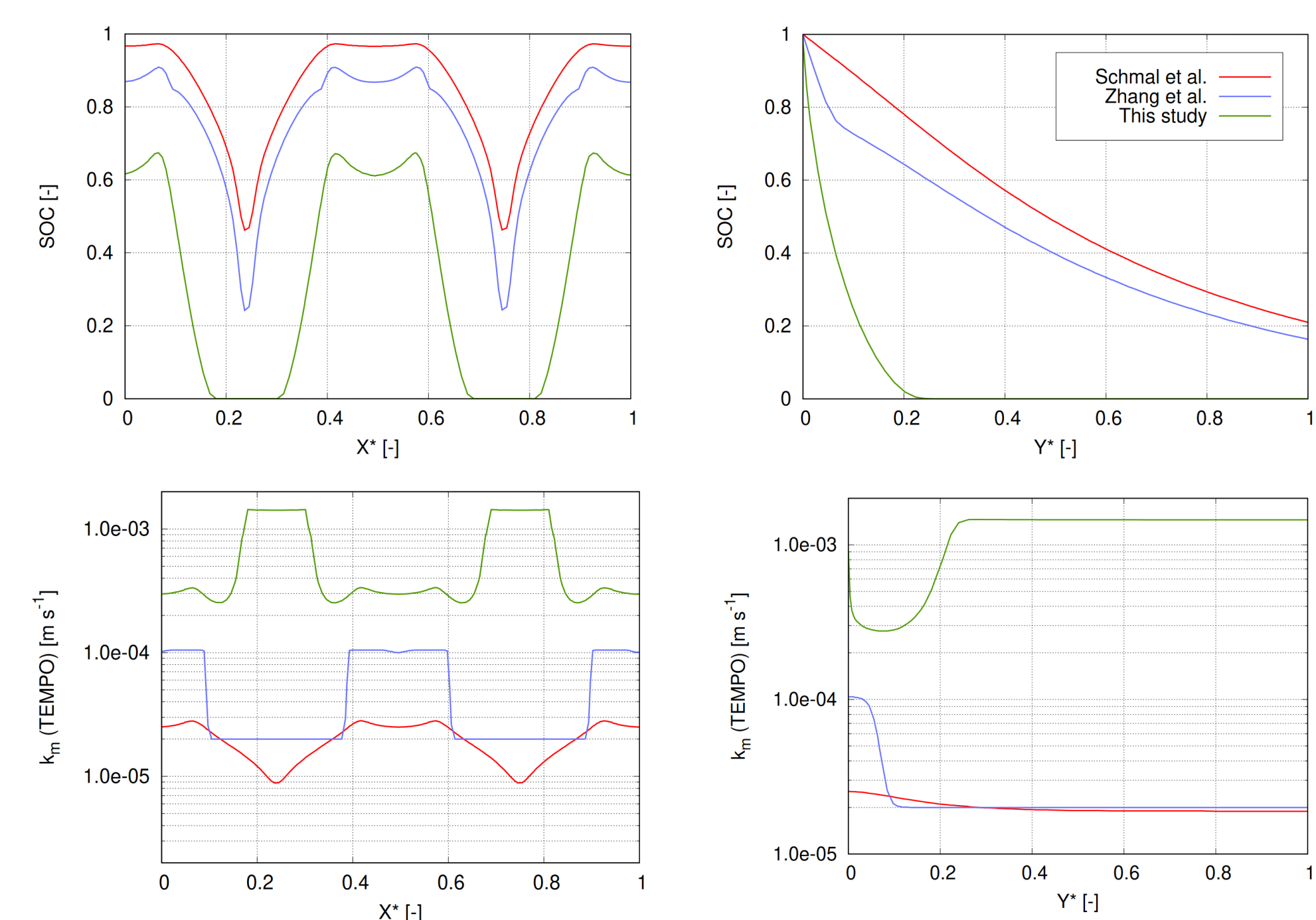
The experiment is marked in red, simulation results are colored in black. To fit the experimental results, the simulated potential is modified with  $75 \text{ mV}$  (gray) arising from membrane polarization.

## MSM mass transfer coefficient extraction

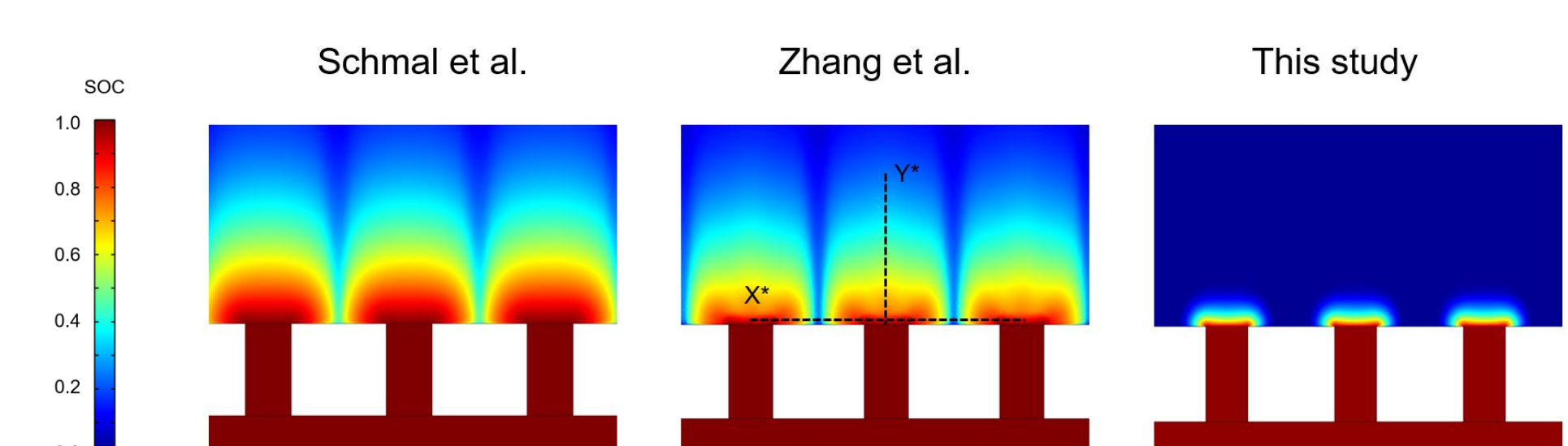


Extracted mass transfer coefficient as function of velocity and SOC (squares) and the corresponding fitting function (line). The initial concentration is  $0.1 \text{ M TEMPO}$  in  $1 \text{ M NaCl}$  and the discharge current density is  $80 \text{ mA m}^{-2}$ . Root mean square error between data and fit is  $2.45 \times 10^{-5}$ . The fit is conducted to be finite at the SOC boundaries.

## Comparison of mass transfer coefficients



Comparison of different mass transfer coefficient approaches and their respective SOC. Horizontal ( $X^*$ ) and vertical ( $Y^*$ ) cut line within the electrode directly after the inlet manifold. The inlet flow rate is  $70 \text{ mL min}^{-1}$  which ensures a flow regime corresponding to  $Re \sim 5 \times 10^{-2}$ . Operating conditions are set to fit the discharge conditions of the coefficient extraction. Except of the inlet manifold for qualitative comparison (below).



Schmal et al.<sup>[3]</sup>  $k_m = 1.6 \times 10^{-4} |\mathbf{u}|^{0.4}$

Zhang et al.<sup>[4]</sup>  $k_m = \left( \left( 1 + \exp\left(-4665 \frac{u}{1 \text{ ms}^{-1}} + 42.302\right) \right)^{-1} + 0.235 \right) \cdot 8.511 \times 10^{-5} \cdot 1 \text{ ms}^{-1}$

## References

- Wolf, A., Baudrin, E., Nirschl, H., (2023) Energy Technology. <https://doi.org/10.1002/ente.202300175>
- A. Wolf, S. Kespe, and H. Nirschl. John Wiley & Sons, Ltd, 2023. Chap. 18, pp. 413–442. doi: <https://doi.org/10.1002/9783527832767.ch18>.
- D. Schmal, J. Van Erkel, and P. J. Van Duin. Journal of Applied Electrochemistry 16.3 (May 1986), pp. 422–430. doi: 10.1007/BF01008853.
- D. Zhang et al. Journal of Power Sources 447 (2020), p. 227249. doi: <https://doi.org/10.1016/j.jpowsour.2019.227249>.

## Acknowledgement

This project has received funding from the European Union's Horizon 2020 research and innovation programme under Grant Agreement no. 875489.



## Contact

Amadeus Wolf, M.Sc.  
Strasse am Forum 8  
76131 Karlsruhe, Germany  
Phone: +49 721 608 45089  
Email: amadeus.wolf@kit.edu

